Reg No.:

Name: 02000CHT204052101 APJ ABDUL KALAM TECHNOLOGICAL UNIVERSITY

Fourth Semester B.Tech Degree Examination July 2021 (2019 Scheme)



Course Code: CHT204

Course Name: HEAT TRANSFER OPERATIONS

	Max. M	arks: 100 Duration:	3 Hour
PART A			
		(Answer all questions; each question carries 3 marks)	Mark
	1	Consider an insulated pipe exposed to the atmosphere. Will the critical radius	3
		of insulation be greater on calm days or on windy days? Why?	
	2	State and write Fourier's law of heat conduction	3
	3	Draw the thermal boundary layer and temperature profile for fluid flowing a	3
		flat plate. (Surface temperature of flat plate is higher than free stream fluid	
		temperature)	
	4	Heat transfer to the ambient air is primarily by natural convection. In which of	3
		the above cases, is the heat transfer coefficient higher and why? A hot	
		horizontal plate is exposed to air by keeping,	
		(i) the hot surface facing (ii) the hot surface facing down	
	5	Explain Leidenfrost point.	3
	6	For film condensation on a vertical plate, Will the heat flux be higher at the top or at the bottom of the plate? Why?	3
	7	What is role of baffles in heat exchangers	3
	8	Define efficiency and capacity ratio of heat exchanger	3
	9	What kind of feeding method is advised if the product is viscous and why?	3
	10	Why steam trap used in evaporators?	3
		PART B	

(Answer one full question from each module, each question carries 14 marks)

Module -1

11 A composite wall (shown below) has uniform temperatures. If the thermal 14 conductivities of the wall materials are: $k_A = 70$ W/m.K, $k_B = 60$ W/m.K, $k_C = 40$ W/m. K, and $k_D = 20$ W/m.K, determine the rate of heat transfer through this section of the wall and the temperatures at the interfaces. (Surfaces normal to

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heat transfer direction are isothermal).



A steam pipe of 10 cm ID and 11 cm OD is covered with an insulating 14 substance k = 1 W/mK. The steam temperature is 200^oC and ambient temperature is 20^oC. If the convective heat transfer coefficient between insulating surface and air is 8 W/m²K, find the critical radius of insulation for this value of rc. Calculate the heat loss per m of pipe and the outer surface temperature. Neglect the resistance of the pipe material.

Module -2

- a) Define thermal boundary layer. Draw and explain hydrodynamic and thermal
 boundary layers when Pr=1, Pr<1 and Pr>1. (Pr=Prandtl number) for flow over
 a flat plate.
 - b) What is use of analogical expressions? Explain Reynolds Analogy stating all 6 assumptions used in derivation.
- 14 a) When 0.6 kg of water per minute is passed through a tube of 2 cm diameter, it 10 is found to be heated from 20°C to 60°C. the heating is achieved by condensing steam on the surface of the tube and subsequently the surface temperature of the tube is maintained at 90°C. Determine the length of the tube required for fully developed flow.

Data: At bulk mean temperature

Density= 995 kg/m³

Viscosity= $0.657 \times 10^{-6} \text{ m}^2/\text{s}$

Pr = 4.340

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k = 0.628 W/mK

Cp = 4178 J/kgK

b) Differentiate Biot number and Nusselt number in heat transfer

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Module -3

Derive Nusselt's equation for condensation on a vertical plate stating all the	14
assumptions.	
The sun emits maximum radiation at $\lambda = 0.52 \mu$. Assuming the sun to be a black	14
body, calculate the surface temperature of the sun. Also calculate the	
monochromatic emissive power of the sun's surface.	
Given:	

$$\lambda_{\rm max} = 0.52 \ \mu = 0.52 \ {\rm x} \ 10^{-6} \ {\rm m}$$

To find:

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(i) Surface temperature, T.

(ii) Monochromatic emissive power, $E_{b\lambda}$

(iii) Total emissive power, E

(iv) Maximum emissive power, Emax

Module -4

- 17 a) Draw a 1-2 shell and tube heat exchanger and mark the parts of heat exchanger
 - b) Heat exchanger temperature profiles of three different purposes are given below. Comment on the heat transfer mechanism in each case. Comment whether to use correction factor (FT) in each case.



Hot chemical products (Cph = 2.5 kJ/kg K) at 600° C and at a flow rate of 30 kg/s are used to heat cold chemical products (Cp = 4.2 kJ/kg K) at 200° C and at a flow rate 20 kg/s in a parallel flow heat exchanger. The total heat transfer is 50 m2 and the overall heat transfer coefficient may be taken as 1500 W/m² K. calculate the outlet temperatures of the hot and cold chemical products.

Module -5

A single effect evaporator is used to concentrate 9070 kg/hr of 20% caustic 14 soda solution to 50% solids. The gauge pressure of steam is 1.37 atm. The

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absolute pressure in the vapor space is 100 mm Hg. There is a BPE of 22.78 °C. The overall heat transfer coefficient is estimated to be 1400 W/m² °C and the feed temperature is 37.8 °C. Calculate the (a) Amount of steam consumed (b) Economy (c) Heating surface required. Data: Enthalpy of feed at 37.8 °C = 127.9245 kJ/kg Enthalpy of thick liquor = 514.0239 kJ/kg Enthalpy of vapour = 2672.46 kJ/kg Heat of vaporization of steam at 1.37 atm = 2184.0201 KJ/ Kg Condensation temperature of steam = 126.11°C

20 a)

Write the material and energy balance of a backward feed triple effect evaporator with a neat sketch

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b) With a neat sketch explain the working of agitated thin film evaporators

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